

**Amendments to the Specification:**

Please replace the paragraph beginning at page 11, paragraph 1 with the following rewritten paragraph:

C1  
-This treatment can be carried out with any catalyst allowing the conversion of saturated sulfur compounds (primarily the compounds of ~~thiophene~~ thiophane type or mercaptan type). It can be carried out, for example, by using a catalyst with a base of nickel, molybdenum, cobalt, tungsten, iron or tin. The treatment is preferably carried out in the presence of a catalyst with a base of nickel, nickel and tin, cobalt and iron, or cobalt and tungsten.

Please replace the paragraph beginning at page 30, paragraph 1 with the following rewritten paragraph:

C2  
-The gasoline that is hydrogenated under the conditions of Example 1 is hydrodesulfurized. A test is performed under the same conditions as those of Example 3, if it is only that the two catalysts are placed in two different reactors and that H<sub>2</sub>S is separated between these two reactors. The effluent of the first reactor is cooled to ambient temperature, and the liquid phase and the gaseous phase are separated; H<sub>2</sub>S of the liquid phase is stripped by a nitrogen stream that makes it possible to eliminate H<sub>2</sub>S to a content of 50 ppm by weight relative to the liquid. The liquid that is thus obtained is then reheated to the temperature of the second catalyst and reinjected in the presence of hydrogen that is introduced with a hydrogen flow rate of 330 l/l of feedstock that corresponds approximately to the flow rate of hydrogen entering the second reactor catalytic zone of Example 3.

Please replace the paragraph beginning at page 31, paragraph 3 with the following rewritten paragraph:

C3  
-The gasoline hydrogenated under the conditions of Example 1 is hydrodesulfurized. 25 ml of catalyst A is placed in a tubular reactor. This reactor is coupled with a second hydrodesulfurization reactor containing 13 ml of catalyst A of Example 1 and 25 ml of catalyst C of Example 3, so that the feedstock first meets catalyst A and then catalyst C. The effluent of the first reactor is cooled to ambient temperature, the liquid phase and the gaseous phase are

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63 separated, and the H<sub>2</sub>S of the liquid phase is stripped by a nitrogen stream allowing to eliminate H<sub>2</sub>S to a content of 50 ppm by weight relative to the liquid. The liquid thus obtained is then reheated to the temperature of the second reactor and reinjected in the presence of hydrogen introduced with a flow rate and under a pressure corresponding to that of the second reactor of Example 4 2. The temperature of the first reactor is indicated in Table 5. The temperature of catalyst A that is present in the second zone is brought to 270°C, and the temperature of catalyst C that is present in the second reactor is brought to 330°C.

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